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65. (Currently amended) The process of claim 1 wherein the polycondensation is carried out in a column reactor is equipped with a heat source located within the reaction medium.

66. (Currently amended) The process of claim 1, wherein the column reactor has 3-30 stages.

67. (Currently amended) The process of claim 1 wherein the column reactor ~~has is~~ ^{has} a vertical column reactor and 4-20 stages.

68. (Currently amended) The process of claim 1 wherein the column reactor has 8-15 stages.

69. (Previously presented) The process of claim 1 wherein the 1,3-propanediol reactant is fed at multiple locations to the reactor.

70. (Previously presented) The process 1 wherein an inert gas is added to the reactor at one or more stages.

71. (Previously presented) The process of claim 1 wherein water vapor is generated as a by-product of the reaction and is removed from the reactor in at least one intermediate stage.

72. (Currently amended) The A continuous process of ~~claim 1~~ making polytrimethylene ether glycol comprising:

(a) providing 1,3-propanediol reactant,

(b) providing polycondensation catalyst; and

(b) polycondensing the 1,3-propanediol reactant to polytrimethylene ether glycol;

wherein the polycondensation is first carried out in at least one prepolymerizer reactor and then polycondensation continued continuously in a column reactor having two or more reaction stages using the polycondensation catalyst, the 1,3-